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JAN 08 2010

Amendments to the Claims

Please amend the claims as follows:

1-30. (Canceled).

31. (New) A process to generate heat, the process comprising:
supplying fuel comprising Fischer-Tropsch derived fuel comprising Fischer-Tropsch product having a density of between 0.65 and 0.8 g/cm³ at 15 °C to an evaporation surface of the evaporator burner oven;
evaporating at least a portion of the fuel into space surrounding the evaporation surface, producing evaporated fuel; and,
combusting at least a portion of the evaporated fuel with oxygen-containing gas to generate heat.
32. (New) The process of claim 31 comprising supplying the fuel to the evaporation surface comprising a wick.
33. (New) The process of claim 31 comprising supplying the fuel to openings through one or more fuel supply conduits.
34. (New) The process of claim 31 further comprising producing a reduced unburned hydrocarbon content compared to combusting a petroleum derived kerosene fuel under the same conditions using the same burner.
35. (New) The process of claim 31 further comprising producing reduced carbon monoxide emissions compared to combusting a petroleum derived kerosene fuel under the same conditions using the same burner.
36. (New) The process of claim 34 further comprising producing reduced carbon monoxide emissions compared to combusting a petroleum derived kerosene fuel under the same conditions using the same burner.
37. (New) The process of claim 31 further comprising producing a reduced Smoke Number compared to combusting a petroleum derived kerosene fuel under the same conditions using the same burner.
38. (New) The process of claim 36 further comprising producing a reduced Smoke Number compared to combusting a petroleum derived kerosene fuel under the same conditions using the same burner.

39. (New) The process of claim 31 wherein the Fischer-Tropsch derived fuel boils for more than 90 wt % between 160 °C. and 400 °C.
40. (New) The process of claim 39 wherein the Fischer-Tropsch product contains more than 80 wt % of iso and normal paraffins, less than 1 wt % aromatics, less than 5 ppm sulfur and less than 1 ppm nitrogen.
41. (New) The process of claim 31 wherein the Fischer-Tropsch derived fuel comprises more than 80 wt % of the Fischer-Tropsch product.
42. (New) The process of claim 31 wherein the Fischer-Tropsch derived fuel comprises one or more additives.
43. (New) The process of claim 31, wherein the Fischer-Tropsch derived fuel comprises an additive selected from the group consisting of an odor marker, a color marker, and a combination thereof.
44. (New) The process of claim 31 wherein the fuel does not contain a metal-based combustion improver and the combusting produces a flame, the process further comprising accurately detecting the flame using an ionization sensor.
45. (New) The process of claim 41 wherein the fuel comprises a color marker and the combusting produces a flame, the process further comprising accurately detecting the flame using a yellow flame detector.
46. (New) The process of claim 31 wherein the Fischer-Tropsch derived fuel comprises a mineral oil fraction and/or a non-mineral oil fraction.
47. (New) The process of claim 41 wherein the Fischer-Tropsch derived fuel comprises a mineral oil fraction and/or a non-mineral oil fraction.
48. (New) A process to generate heat, the process comprising:
supplying fuel comprising Fischer-Tropsch derived fuel comprising Fischer-Tropsch product having a density of between 0.65 and 0.8 g/cm³ at 15 °C to an evaporation surface of the evaporator burner oven;
evaporating at least a portion of the fuel into space surrounding the evaporation surface, producing evaporated fuel; and,
combusting at least a portion of the evaporated fuel with oxygen-containing gas to generate heat, the combusting producing increased efficiency compared to

combusting a petroleum derived kerosene fuel under the same conditions using the same burner.

49. (New) A process to generate heat, the process comprising:
supplying fuel comprising Fischer-Tropsch derived fuel comprising Fischer-Tropsch product having a density of between 0.65 and 0.8 g/cm³ at 15 °C to an evaporation surface of the evaporator burner oven;
evaporating at least a portion of the fuel into space surrounding the evaporation surface, producing evaporated fuel; and,
combusting at least a portion of the evaporated fuel with oxygen-containing gas to generate heat;
wherein, compared to combusting a petroleum derived kerosene fuel under the same conditions using the same burner, the combusting produces increased efficiency and a reduced unburned hydrocarbon content.
50. (New) The process of claim 49 further comprising producing reduced carbon monoxide emissions compared to combusting a petroleum derived kerosene fuel under the same conditions using the same burner.
51. (New) The process of claim 49 further comprising producing a reduced Smoke Number compared to combusting a petroleum derived kerosene fuel under the same conditions using the same burner.
52. (New) The process of claim 50 further comprising producing a reduced Smoke Number compared to combusting a petroleum derived kerosene fuel under the same conditions using the same burner.